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Comprehensive modelling study of ozonolysis of oleic acid aerosol based on real-time, online measurements of aerosol composition

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Key Points:

- Extractive Electrospray Ionisation Mass Spectrometry can be used to assess reaction kinetics in oleic acid aerosols.
- The most important sinks for Criegee intermediates formed during oleic acid ozonolysis are isomerization and secondary ozonide formation.
- The Pretty Good Aerosol Model can reproduce measurements of evolving reactant loss, product formation and particle size change.
Abstract

The chemical composition of organic aerosols profoundly influences their atmospheric properties, but a detailed understanding of heterogeneous and in-particle reactivity is lacking. We present here a combined experimental and modelling study of the ozonolysis of oleic acid particles. An online mass spectrometry (MS) method, Extractive Electrospray Ionization (EESI), is used to follow the composition of the aerosol at a molecular level in real time; relative changes in the concentrations of both reactants and products are determined during aerosol aging. The results show evidence for multiple non first order reactions involving stabilized Criegee intermediates, including the formation of secondary ozonides and other oligomers. Offline Liquid Chromatography (LC) MS is used to confirm the online MS assignment of the monomeric and dimeric products. We explain the observed EESI-MS chemical composition changes, and chemical and physical data from previous studies, using a process-based aerosol chemistry simulation, the Pretty Good Aerosol Model (PG-AM). In particular, we extend previous studies of reactant loss by demonstrating success in reproducing the time dependence of product formation and the evolving particle size. This advance requires a comprehensive chemical scheme coupled to the partitioning of semivolatile products; relevant reaction and evaporation parameters have been refined using our new measurements in combination with PG-AM.

1. Introduction

Organic compounds comprise a significant fraction of fine aerosol particle mass in the atmosphere [Murphy et al., 2006]. The chemical composition of both directly emitted, primary organic particles and those formed by secondary processes is transformed continuously in the atmosphere [Ziemann and Atkinson, 2012], with contingent but poorly understood influences on the Earth’s climate [Boucher et al., 2013] and human health [Pope et al., 2009].

Heterogeneous and in-particle reactions of organic compounds are particularly poorly understood. In-particle reactivity is complicated by the strong influence of composition (aerosol water content, ionic strength, organic functional group concentrations etc.) on observed reactions and products [Kroll and Seinfeld, 2008]. In addition, identifying individual reaction pathways in chemically complex mixtures is a difficult analytical and conceptual challenge [Noziere et al.,
Previous studies have attempted to quantify reactive uptake to particles [Liggio and Li, 2006; Rudich et al., 2007] and lifetimes of marker compounds in aerosols with respect to heterogeneous oxidation [Robinson et al., 2007; Zhao et al., 2014]. The thermodynamic viability of some reversible accretion reactions in particles have also been assessed [Barsanti and Pankow, 2005, 2006]. In general, however, there is a need for detailed studies which elucidate the major products, channels and pathways of in-particle reactions as a starting point for assessing their atmospheric implications.

This study presents a combined measurement and modelling approach to understand product formation mechanisms and kinetics during the heterogeneous ozonolysis of oleic acid (OA) particles. Oleic acid is a low vapor pressure unsaturated fatty acid. Fatty acids are an important class of compounds in the atmosphere [Rogge et al., 1993; Mochida et al., 2002; Wang et al., 2006] and moreover OA aerosols have become an important test case for our understanding of heterogeneous and in-particle reactions [Ziemann, 2005; Zahardis and Petrucci, 2007]. Here, time-resolved molecular composition measurements are obtained from a recently developed mass spectrometry (MS) technique, Extractive Electrospray Ionization (EESI) [Gallimore and Kalberer, 2013]. EESI-MS is an online method capable of extracting and ionizing organic analytes from aerosols to produce molecular ions with minimal fragmentation. Intensity changes of reactant and product ions can be related to concentration changes in particles.

A few explicit or near-explicit models of organic aerosol chemistry have been described in recent years [Griffiths et al., 2009; McNeill et al., 2012; Berkemeier et al., 2013; Houle et al., 2015]. These provide a flexible and rigorous framework in which to test our understanding of aerosol chemistry and transport phenomena, in so far as relevant physico-chemical data are available. Comparison with detailed measurements is essential for model validation; their predictive ability can then be used to probe experimentally inaccessible phenomena, refine uncertain parameters and provide a link between experiment and larger-scale models. Here, we use the Pretty Good Aerosol Model (PG-AM) adapted from Griffiths et al. [2009]. Reaction, diffusion and interfacial transport are represented explicitly in the model based on evaluated physical parameters derived from the literature. We compare to a range of previous observations of oleic acid loss and particle size change. We have also built a detailed chemical mechanism to capture the time
dependence of multi-generational product formation observed by EESI-MS, in particular elucidate the fates of Criegee intermediates (CIs) formed during ozonolysis.

2. Methods

2.1. Aerosol Flow Tube experiments

Oleic acid particles were generated in the laboratory and reacted with ozone according to the scheme in Figure 1. A solution of 3 mmol/L oleic acid (99%, Sigma Aldrich) in ethanol (analytical reagent grade, Fisher) was prepared for use in a custom built constant-output nebuliser. The nebuliser was supplied with nitrogen (oxygen-free, BOC) at a pressure of 2 bar and output flow rate of 0.65 L/min. A charcoal denuder was employed to remove ethanol from the particles, although small amounts (we estimate a few percent on a molar basis) were detected in the MS analysis. No water was added to the system and the measured relative humidity (RH) was less than 5% throughout the experiments. Ozone was produced by flowing synthetic air (zero grade, BOC) through a photolysis tube containing a mercury UV lamp (Pen-Ray 3SC-9, UVP) at 0.65 L/min. The concentration of ozone was varied by partially covering the lamp with an aluminum sheath. It was varied between 8 and 22 ppm, determined after mixing with the aerosol flow using a UV photometric ozone analyser (Thermo Scientific model 49i). Experiments were performed in an air-conditioned laboratory at 20 °C.

A series of steady-state reaction times between oleic acid particles and ozone were established using five by-passable flow tubes. The aerosol and ozone were mixed into a 4 mm inner diameter PTFE tube. The Reynolds number (Re) of the fluid flow was calculated as Re ~110 and a laminar mixing time < 0.1 s was therefore estimated based on Keyser [1984]. The reaction time was estimated by dividing the total reaction volume by the volumetric flow rate. The total reaction volume could be varied between 0.1-5.4 L resulting in reaction times of ~3-140 s. A second charcoal denuder was employed after the reaction volumes to remove any remaining ozone and gas-phase organic species. The polydisperse aerosol size distribution was monitored using a scanning mobility particle sizer (TSI model 3936). A single mode was observed with a geometric standard deviation of 1.8, and a typical particle mass loading of 5 mg/m³. To account
for the full aerosol volume and surface area distributions, an “effective” average particle radius, \( r_{\text{eff}} = 3V/S \), was calculated [Stewart et al., 2004]. For fresh particles, \( r_{\text{eff}} \) was determined to be 250 nm and was used as the particle radius in the model simulations described below.

**Figure 1:** Schematic diagram of laboratory setup for ozonolysis of oleic acid aerosol and chemical characterization. The ozone and aerosol were rapidly mixed so the exposure time was defined by the variable reaction volume between mixing and the second denuder. The steady state aerosol composition for a particular ozone exposure was acquired using EESI-MS, and the ion source was flushed with clean air between samples and “blank” spectra were recorded during this time.

### 2.2. EESI-MS operation

The EESI source is described in detail by Gallimore and Kalberer [2013]. Briefly, it consists of a custom-built aerosol injector and housing which is interfaced with a commercially-available electrospray ionisation (ESI) source (Thermo Scientific HESI-II). The primary solvent electrospray was a water-methanol 1:1 mixture (Optima LC-MS grade solvents, Fisher Scientific) containing 0.05% formic acid (90%, Breckland Scientific) and was operated in negative ionisation mode with a spray voltage of \(-3.0\) kV. The aerosol injector delivered particles at a flow rate of 1 L/min into the primary solvent spray. Particle-droplet collisions dissolve the aerosol analytes, which are ionised and ejected into the gas phase by a Coloumb explosion mechanism typical for electrospray ionisation.
The EESI-MS acquisition was varied between blank and sample measurements from the aerosol flow tube setup. Prior to blank measurements, air was flushed through the source for 15 minutes to remove particles from the previous sample while the aerosol flow was diverted to a vent. During sample measurements, the flushing air flow was switched off and the aerosol diverted into the EESI source. This assured a constant flow of 1 L/min into the source was maintained at all times. Mass spectrometry measurements were made using an ultra-high resolution mass spectrometer (Thermo Scientific LTQ Orbitrap Velos). The high mass accuracy (<2 ppm) and resolution (m/Δm = 100 000 at m/z 400) of this instrument means that unambiguous molecular formula assignments for reaction product ions are usually achieved.

Measurements were repeated three times for each reaction time and the standard deviation of the relative peak intensities in the mass spectra were calculated (uncertainty on the ordinate in kinetic plots). The largest uncertainty related to ozone exposure (abscissa in kinetic plots) was the observation of limited quantities of oleic acid oxidation products (5-7%) even before deliberate ozone exposure. This prior exposure (for example in the nebulizer or during sample preparation) was estimated by extrapolating best fit curves of the major products (azaleic acid (AA), 9-oxononanoic acid (9-ON) and nonanoic acid (NA)) back to a hypothetical “zero” intensity where they intercepted the ozone exposure axis. A prior exposure of $1.6 \times 10^{-5}$ atm s was estimated and used in Figures 4 and 5.

### 2.3. Numerical Simulation of aerosol processes

In support of the measurements, we compared the results against a numerical model of reactive uptake of ozone by oleic acid aerosol. The Pretty Good Aerosol Model (PG-AM) describes the coupled uptake from and evaporation to the gas phase, as well as coupled reaction/diffusion processes occurring within the aerosol.

The approach is based on the work by Griffiths et al., [2009] used in the study of reactive uptake of N$_2$O$_5$, in which the aerosol particle is treated as a series of concentric equal-volume shells, and uptake is modelled as a series of coupled reaction-diffusion equations. For this work, diffusion is parameterized as in Griffiths et al., [2009] and the reactions treated by the coupled equations were modified to include a mechanism for oleic acid ozonolysis including higher-order reactions between products, as described in section 2.4. The model is based as far as possible on a
physically-based description of the chemistry and transport, and uses as input experimentally accessible parameters such as diffusion coefficients and solubilities. Table S1 gives the parameters employed here.

The model is written in Mathematica v10 (Wolfram) and the equations integrated forward in time using the NDSolve routine. For this work, uptake to a single representative aerosol particle was studied. The radius was set to the effective radius of the measured aerosol distribution ($r_{\text{eff}} = 3V/S_t$), and the time-dependence of aerosol components simulated for an initial pure oleic acid particle on exposure to the measured ozone field. When comparing with our experiments, a degree of uncertainty may be introduced by size-dependent uptake from a polydisperse aerosol ensemble.

2.4. Model mechanism for ozonolysis of oleic acid aerosol

The formation of low molecular weight C_9 products from oleic acid ozonolysis has been reviewed in the literature [Ziemann, 2005; Zahardis and Petrucci, 2007; Lee et al., 2012] and is outlined in Figure 2(a). The ozone-alkene cycloaddition produces a short-lived primary ozonide (POZ) which decomposes into an aldehyde and a rapidly stabilised Criegee intermediate (CI). We assume CIs are stabilised in the subsequent discussion. Large nonanal (NN) yields have been observed in previous studies [Vesna et al., 2009; Wang et al., 2016] suggesting that the NN + CI-187 route is favored over the 9-oxononanoic acid (9-ON) + CI-157 route. Formation of nonanoic and azaleic acids (NA, AA) from CIs is often described as a pseudo-unimolecular isomerization [Ziemann, 2005] ($k_a$ in Figure 2(b)) with a plausible mechanism proposed by Zahardis et al., [2005]. The model parameters $k_{\text{OA} + \text{O}_3}$, $\chi$ and $k_a$ were estimated from the literature and are detailed in Table S1.

The products formed from secondary reactions depend critically on the fates of the CIs. A particular focus of our work is to better constrain the relative rates of these CI reactions. Although a large number of reactions have been proposed in the literature, many of the proposed mechanisms are speculative and the kinetics essentially unknown. We proceeded by introducing simplifications to reduce parametric uncertainty in the model and align our mechanism with the main dimeric products observed in our EESI-MS and LC-MS analysis (Figure 2(b)), and previous studies [Zahardis et al., 2005; Reynolds et al., 2006; Lee et al., 2012]. This assigned a
single rate constant to all CI + carboxylic acid ($k_b$) and CI + aldehyde ($k_c$) reactions. Other reactions were omitted altogether. CI self-reactions, second order in [CI], were neglected due to the short CI lifetime and hence low steady state [CI]. The kinetics of CI + alkene reactions have not been studied experimentally but the theoretical study of Vereecken et al., [2014] concluded that they are orders of magnitude slower than reactions with carboxylic acids and carbonyls for a given CI. However, we note the very recent study of Wang et al., [2016] and the earlier work of Katrib et al., [2004] which point to a potentially significant role for this reaction.

Omission of these potential CI sinks in the model may have led to overestimation of [CI] and hence underestimation of $k_b$ and $k_c$ which were varied to obtain a good fit to the measured data in the model. In addition, the missing CI + alkene reaction possibly underestimates the oleic acid loss rate. However, this simplified mechanism minimizes the parametric uncertainty associated with tuning the model rate constants to match the observations given the limited number of assigned products. We also believe that it is chemically sensible to lump the rate constants based on functional group reactivity.
Figure 2: Chemical mechanism of oleic acid ozonolysis implemented in the model. (a) Primary C\textsubscript{9} products and Criegee intermediates formed from the initial ozone-alkene cycloaddition. (b) Reactions of the Criegee intermediates: isomerisation to form carboxylic acids ($k_a$) and reactions with other functional groups to form dimers ($k_b$ and $k_c$). $k_{OA+O_3}$, $\chi$ and $k_a$ were estimated from the literature, $k_b$ and $k_c$ were adjusted to achieve the best fit to the measurements. We assign structures in blue to observed m/z, but assume the proposed black structures (intermediates and volatile products) would not be observed.

3. Experimental results and discussion

3.1. Product determination by mass spectrometry
A typical mass spectrum obtained from the EESI-MS analysis of oleic acid aerosol, partially oxidized with ozone, is given in Figure 3. The spectrum was acquired in negative ionization mode, meaning that functional groups which are readily deprotonated, such as carboxylic acids, are efficiently detected. Unreacted oleic acid was detected at \( m/z \) 281.2486. The peaks at \( m/z \) 157.1234, 171.1027 and 187.0976 were assigned as the three low volatility C\(_9\) products from Figure 2: nonanoic acid (NA), 9-oxononanoic acid (9-ON) and azaleic acid (AA). The other C\(_9\) product, nonanal (NN), is highly volatile and has been seen to partition into the gas phase [Vesna et al., 2009] causing evaporative size changes [Dennis-Smither et al., 2012]. In addition, its aldehyde functional group would not be readily ionized by deprotonation.

![Mass spectrum of partially oxidized oleic acid aerosol acquired using EESI-MS](image)

**Figure 3:** Mass spectrum of partially oxidized oleic acid aerosol acquired using EESI-MS. The initial particle-phase products of oleic acid ozonolysis, nonanoic acid (NA), 9-oxononanoic acid (9-ON) and azaleic acid (AA) are detected along with unreacted oleic acid (OA). The inset graph is an expansion of the region above \( m/z \) 275 which includes assignments of dimer products resulting from the reaction of primary products with Criegee intermediates. \( m/z \) intensities will be a function of both analyte concentration and ionization efficiency; we relate relative intensity changes to relative concentration changes in the aerosol, but note that the most intense peaks are not necessarily the most abundant aerosol species. The peaks marked (*) are cut off on the expanded scale.

The Criegee intermediates CI-157 and CI-187 are isobaric with NA and AA but we assume that, if detected, they do not make a significant contribution to the observed peak intensities due to their low concentrations. There is a small additional “monomer” peak at \( m/z \) 203.0925, also
observed by Reynolds et al., [2006] which increases in intensity with ozone exposure and has a molecular formula consistent with a hydroperoxide product. This could form following decomposition of higher molecular weight products or reaction of the CIs with trace amounts of water. Other peaks in this region were not assigned and may be fragments or impurities from the electrospray solvent.

High molecular weight products are shown in the inset spectrum in Figure 3. The molecular formulae of the ions labelled “D” are consistent with dimers formed via CI-monomer reactions. Such products have been proposed in the literature and observed in previous studies [Zahardis et al., 2005; Reynolds et al., 2006; Lee et al., 2012]. Our mechanism includes formation of these products as given in Figure 2(b). Specific possible structures for these species are given in Table S2. While the very recent study of Wang et al., [2016] proposes a route to high molecular weight products via CI + alkene reactions, the proposed C_{27} products were not identified in our measurements. The ions discussed here are listed in Table 1 for reference, along with potential structures and formation reactions.

<table>
<thead>
<tr>
<th>m/z</th>
<th>Name and abbreviation</th>
<th>Possible structures (neutral)</th>
<th>Formation reaction</th>
</tr>
</thead>
<tbody>
<tr>
<td>157.1027</td>
<td>Nonanoic acid (NA)</td>
<td></td>
<td>CI-157 isomerisation (k_a)</td>
</tr>
<tr>
<td>171.1027</td>
<td>9-Oxnonanoic acid (9-ON)</td>
<td></td>
<td>OA + O_3 (k_{OA+O3})</td>
</tr>
<tr>
<td>187.0976</td>
<td>Azaleic acid (AA)</td>
<td></td>
<td>CI-187 isomerisation (k_a)</td>
</tr>
<tr>
<td>281.2486</td>
<td>Oleic acid (OA)</td>
<td></td>
<td></td>
</tr>
<tr>
<td>329.2334</td>
<td>Dimer-329 (D-329)</td>
<td></td>
<td>9-ON + CI-157 (k_c) Secondary ozonide (SOZ)</td>
</tr>
<tr>
<td>345.2283</td>
<td>Dimer-345 (D-345)</td>
<td></td>
<td>NA + CI-187 (k_b) Hydroperoxide (α-AAHP)</td>
</tr>
</tbody>
</table>
Table 1: Species detected via mass spectrometry in Figure 3 and Figure S1 which are products of ozonolysis considered in the model. Possible structures and the relevant formation reactions from Figure 2 are also listed.

Since LC-MS analysis involves separation and ionization of individual species according to retention time, it can be used to confirm that ions detected in direct infusion techniques correspond to stable molecular structures. LC-MS was applied here to oxidized oleic acid aerosol collected offline (described in the Supplementary Information, Figure S1). Distinct LC-MS peaks were identified for \textit{m/z} 375.2024 and \textit{m/z} 359.2075. The time dependence of these dimer ions in EESI-MS were therefore compared to the model calculations alongside the monomers. Corresponding chemistry for D-329 and D-345 was also included in the model but distinct LC-MS peaks could not be identified. Given the low abundance of these peaks in direct EESI-MS, it may be that they are lost in the LC-MS baseline, or are not as stable during aerosol collection, storage and extraction. The measured time dependence of \textit{m/z} 329.2334 and 345.2283 was therefore not used to constrain the model performance.

### 3.2. Kinetics of oleic acid loss

The kinetics of the heterogeneous reaction between oleic acid particles and ozone were monitored using EESI-MS. Relative particle-phase concentration changes were determined from relative intensity changes of reactant and product ions in the MS. The validity of this approach was demonstrated in Gallimore and Kalberer [2013] and is extended here to an ensemble of
particles whose composition is changing as a function of time. Figure 4(a) shows the intensity of $m/z$ 281.2486, assigned to deprotonated oleic acid [OA – H]$^-$, as a function of ozone exposure in the flow tube. The OA signal intensity is scaled relative to the spectrum of unreacted OA particles (i.e. before deliberate ozone exposure). Our data are all for conditions where only a small fraction of gas-phase ozone ($< 10\%$) is consumed by reactive uptake. Data from three different ozone concentrations are mapped onto a consistent ozone exposure ($P_{O3,t}$) scale; the individual time series are provided in the supplementary information (Figure S2).
Figure 4: (a) Relative intensity of m/z 281.2486 ion corresponding to \([\text{OA} - \text{H}]^-\) as a function of ozone exposure \((P_{O_3}, t)\). On this scale, the data map well onto a single exponential best fit curve, suggesting that OA loss scales linearly with \([\text{O}_3 (g)]\).

(b) Time series for 8ppm ozone for ions assigned to primary C\(_9\) products of oleic acid ozonolysis: nonanoic acid (NA), 9-oxononanoic acid (9-ON), and azaleic acid (AA). The ion intensities were scaled to their value at 140 s when essentially all of the oleic acid was depleted, and hence the symbols for NA, 9-ON and AA overlap at this time. The curve represents a hypothetical first-order production term from oleic acid; this describes NA and AA relatively well at short times but does not capture the behavior of 9-ON.

The consensus from previous particle-phase observations, based on the functional form and pronounced size dependence of OA loss, is that ozone reacts rapidly once accommodated onto oleic acid particles \([\text{Morris et al., 2002; Smith et al., 2002; Hearn and Smith, 2004; Hearn et al., 2005; Ziemann, 2005}]\). The exponential fit to all of our data in Figure 4(a) is consistent with the formulation of \textit{Hearn et al.} [2005] for reaction in a surface film (case 3 kinetics):

\[
\frac{[\text{OA}]}{[\text{OA}]_0} = \exp\left(-\frac{3\delta^2}{r} K_{H,O_3} k^{II} P_{O_3} t\right) \tag{1}
\]

Where \(\delta\) is the thickness of the surface film, \(r\) is the particle radius, \(K_{H,O_3}\) is the Henry’s law coefficient for ozone in oleic acid, \(k^{II}\) is the ozonolysis rate constant in the film, \(P_{O_3}\) is the ozone partial pressure and \(t\) is the reaction time. Our data from three different ozone concentrations are well described by a single fit to Equation (1) in Figure 4(a). Consistent with this formulation, our OA loss rate is a linear function of ozone concentration in the flow tube; we extracted pseudo-first order loss rates for each concentration from Figure 4(a) which are listed in Table S2. Previous data have been presented on an ozone exposure scale \([\text{Morris et al., 2002; Hearn and Smith, 2004}]\), but to our knowledge this linearity in \([\text{O}_3 (g)]\) has not been explicitly demonstrated before. We note that any possible secondary losses of oleic acid from other reactants such as Criegee intermediates do not perturb pseudo-first order OA losses and are therefore likely of minor importance.

The oleic acid loss measurements also enable us to derive a reactive uptake coefficient for ozone onto the aerosols. We follow the approach of \textit{Hearn et al.} [2005] for reaction in a surface film and calculate \(\gamma = 5 \times 2 \times 10^{-4}\). This is relatively low compared to \(\gamma ~ 8 \times 10^{-4}\) recommended by the review of \textit{Zahardis and Petrucci} [2007], but is within the combined experimental
uncertainty. This compares well to a recent determination by Al-Kindi et al., [2016] and lower values have been reported in other studies [Dennis-Smither et al., 2012].

3.3. Kinetics of product formation

EESI-MS allows us to monitor changes in a variety of products, including complex secondary species which are difficult to analyse using many alternative approaches. Now that we have established that the oleic acid loss rate is first order in \([O_3 \text{(g)}]\), we present the remaining data as a function of time rather than ozone exposure for more explicit comparison with PG-AM. We consider first the primary C9 products, and Figure 4(b) shows measured time series for nonanoic acid (NA), 9-oxononanoic acid (9-ON) and azaleic acid (AA) for particles exposed to the lowest of the three ozone concentrations, 8 ppm. In this case ion intensities are scaled to a nominal final value when essentially all of the oleic acid had reacted.

These products are formed from the initial ozone-alkene reaction, either directly or via CI-isomerization (Figure 2(a)). If we assume the particle-phase CI lifetime is short, we might therefore expect the products to all exhibit the same time dependence based on the characteristic timescale for oleic acid loss \(k_1 = 0.050 \text{ s}^{-1}\) from Table S3. The black curve in Figure 4(b) illustrates a calculated first-order production term alongside the measurements. We ascribe differences between the species, and deviation from this curve, to non-first order processes, specifically oligomer formation reactions. The NA and AA data show a very similar time dependence which is close to the calculated curve over most of the reaction, although some differences can be seen at 40 s. This suggests that the loss processes for these species are relatively small. By contrast, the relative concentration of 9-ON deviates from this first-order behavior. We hypothesize that this is due to a bimolecular sink for 9-ON, such as reaction with CI:

\[
\frac{d[9-\text{ON}]}{dt} = k_{OA+O_3}[O_3][OA] - k_c[9-\text{ON}][\text{Cl}] \quad (2)
\]

The production term is unchanged from the black curve in Figure 4(b) and will be largest at the start of the reaction. However, the loss term will increase as 9-ON builds up. On a relative concentration scale, the net effect of this scenario is to make the product time series approach a maximum more rapidly, consistent with the observed 9-ON profile. We quantitatively assess the
importance of this reaction and other particle-phase processes using an explicit numerical aerosol model in the following section.

4. Model simulations of experimental observations

4.1. EESI-MS data

To better understand the time dependence of our aerosol chemical composition measurements, we introduce a model which explicitly simulates the underlying processes relevant to organic aerosol aging, the Pretty Good Aerosol Model (PG-AM). This framework also allows us to investigate other observations such as the size-dependent reactivity of oleic acid particles [Morris et al., 2002; Smith et al., 2002] and particle volume changes as a consequence of ozone uptake and product evaporation [Dennis-Smith et al., 2012]. Figure 5 shows modelled time series for oleic acid and a range of primary and secondary products alongside the EESI-MS measurements. The oleic acid losses (Figure(a)) are captured well by the model using the literature parameters specified in Table S1. The accommodation coefficient $\alpha_{O3}$ is a poorly constrained parameter for this system, and $\alpha_{O3} = 10^{-3}$ was found to give a good fit to the data in Figure 5(a) and for the higher ozone concentrations (Figure S3).

The model shows a strong radial gradient in $[O_3 \text{ (l)}]$ during the simulation (Figure S4) which is consistent with the picture of rapid ozone reaction following accommodation to the particle. As a consequence, the modelled oleic acid loss rate exhibits a profound particle size dependence. We characterized the competition between ozone diffusion through the particle and reaction with an oleic acid molecule in terms of a reacto-diffusive length, $l = D_{O3}/k_{O3+OA}[OA]$. For $r_{eff} = 250$ nm used here, we obtained $l < 8$ nm for the early part of the reaction, indicating that the ozone remains confined to the outer few percent of the particle until most of the oleic acid is consumed. This agrees well with an experimental estimate of reacto-diffusive length of 10 nm [Morris et al., 2002]. The oleic acid, meanwhile, shows only small gradients due to rapid bulk diffusion, in agreement with the modelling study of Shiraiwa et al. [2010] and consistent with particles remaining liquid throughout ozonolysis [Hosny et al., 2016].

We also simulated product formation and secondary chemistry occurring in the particles. Since the rates of oligomer formation reactions are not at all known, we proceeded by fixing $k_a = 500$ s$^{-1}$.
based on Welz et al. [2012], and varying the oligomerization reaction rates \( k_b \) and \( k_c \) to obtain the best fit to the MS data. We found that the model was not sensitive to the absolute magnitude of \( k_a \), provided \( k_a \gg k^1 \).

Figure 5: Modelled concentrations as a function of time for (a) oleic acid (OA), (b) nonanoic acid (NA) and azaleic acid (AA), (c) 9-oxononanoic acid (9-ON) and (d) dimer products, dimer-359 and dimer-375. EESI-MS measurements with 8 ppm ozone are included as discrete points and both model and experimental results are scaled to aid comparison. The model shows a close fit to the measured OA (a) and primary product ((b) and (c)) data, and reasonable agreement for the dimer products (d). NA and AA (b) have the same modelled time dependence owing to the symmetry of the mechanism (Figure 2). The dashed line in (c) represents a simulation with the dimer chemistry switched off, and the dashed line in (d) includes a unimolecular sink for D-359 \( (k_{\text{sink}} = 0.01 \text{ s}^{-1}) \) as a proxy for further dimer reactions.

Agreement between the modelled and measured concentrations was found for all of the product species (Figure 5(b)-(d)), given the experimental and parametric uncertainty involved in this comparison. In particular, the characteristic difference in the 9-ON time series compared to the
other primary products noted in Figure 4(b) was reproduced by including the oligomerization
reactions described in Figure 2(b).

9-oxononanoic acid contains an aldehyde functional group as well as the acid group also present
in azaleic acid and nonanoic acid. We therefore found the predominant reaction of 9-ON with
Criegee intermediates to be via the aldehyde group \((k_c)\), with a relatively lower rate of CI-acid
reaction \((k_b)\) for all three \(C_9\) products. The dashed line in Figure 5(c) shows the simulated 9-ON
profile with oligomerization switched off, a demonstrably poorer agreement. The products of CI-
aldehyde reactions are secondary ozonides (SOZs), and our results are consistent with evidence
from the solution-phase literature that SOZs form in high yields [Geletneky and Berger, 1998;
Carey and Sundberg, 2008]. However, they contrast with the findings of Mochida et al. [2006]
who reported that the highest dimer yields from oleic acid ozonolysis result from CI-acid
reactions.

Since the model is not sensitive to the absolute magnitude of \(k_a\), the relative rates \(k_b/k_a\) and \(k_c/k_a\)
determine the fate of the CIs in the particle, specifically the branching between isomerization and
oligomerization. We found \(k_b/k_a = 0.3 \, \text{M}^{-1}\) and \(k_c/k_a = 2 \, \text{M}^{-1}\) respectively gave good fits to the
primary product time series (Figure 5(b) and (c)).

Figure(d) shows the modelled dimer concentrations, which show reasonable agreement with the
experimental values. We found that the modelled profiles were only weakly sensitive to the
relative rates \(k_b/k_a\) and \(k_c/k_a\) and so we used the primary product time series to constrain these
ratios. The simulated D-359 profile is initially too low, possibly as a consequence of missing
reactions which consume the dimer. The dashed line in Figure 5(d) shows a model run with a
pseudo first order dimer loss included \((k_{\text{sink}} = 0.01 \, \text{s}^{-1})\) as a proxy for possible further
decomposition or oligomerization reactions. This improves the agreement for D-359 in an
analogous manner to 9-ON, but the nature of this removal could not be reliably identified from
the observed products.

### 4.1. Simulation of other experimental data

A number of previous studies have presented measurements amenable to process modelling. We
focus on three experimental studies which present explicit time dependent measurements of oleic
Acid concentration changes [Hearn and Smith, 2004; Ziemann, 2005; Dennis-Smither et al., 2012]. These studies span a range of particle sizes, reaction times and ozone concentrations and so present a test of the model performance. The studies are summarized in Table 2. In each case, the model parameters were as used as presented in Table S1, while \( \alpha_{O3} \) was adjusted to obtain a good fit to the oleic acid loss measurements.

<table>
<thead>
<tr>
<th>Study</th>
<th>Particle radius (nm)</th>
<th>[O(_3)] (ppm)</th>
<th>Model parameters</th>
<th>Experimental</th>
</tr>
</thead>
<tbody>
<tr>
<td>This work</td>
<td>~ 250</td>
<td>8-22</td>
<td>Base case (Table S1)</td>
<td>Aerosol ensemble from nebulizer (ethanol solution); flow tube; EESI-MS</td>
</tr>
<tr>
<td>Ziemann [2005]</td>
<td>~ 200</td>
<td>2.8</td>
<td>( \alpha_{O3} = 2 \times 10^{-3} )</td>
<td>Aerosol ensemble by homogeneous nucleation; smog chamber; TDPBMS</td>
</tr>
<tr>
<td>Hearn and Smith [2004]</td>
<td>~ 400</td>
<td>100</td>
<td>( \alpha_{O3} = 1.5 \times 10^{-3} )</td>
<td>Aerosol ensemble from nebulizer (pure OA); flow tube; Aerosol CIMS</td>
</tr>
<tr>
<td>Dennis-Smither et al., [2012]</td>
<td>4580 (core-shell(^*))</td>
<td>6</td>
<td>( \alpha_{O3} = 5 \times 10^{-4} )</td>
<td>OA coagulation with single NaCl core(^*); optical tweezers; Raman and Mie scattering</td>
</tr>
</tbody>
</table>

Table 2: Summary of experimental studies of oleic acid aerosol ozonolysis containing explicit time series for oleic acid loss. The measurements were compared to model simulations under the same conditions and the best agreement was obtained by adjusting the accommodation coefficient for ozone, \( \alpha_{O3} \), as a proxy for experimental and parametric uncertainty. (*) The particles consisted of a liquid oleic acid droplet of the specified total radius, containing an unreactive sodium chloride inclusion of approximately 2 micron radius (spherically equivalent size).
In general, the model does well in reproducing these observations over a range of particle sizes (~200-5000 nm) and oxidation timescales (seconds-10s of minutes) using the same diffusion and reaction parameters as before. Figure 6(a) shows oleic acid loss data for the Dennis-Smith et al., [2012] study, for a single micron-sized particle. We were able to reproduce other studies to a similarly high degree of agreement, and the time series for Hearn and Smith [2004] and Ziemann [2005] are presented in Figures 6(b) and (c) respectively. We feel that close model agreement with a range of measurements helps to rationalize previous observations and provide a more coherent picture of the ozonolysis of oleic acid particles with respect to relevant physico-chemical parameters (Table S1).

The modified $\alpha_{O3}$ values can be seen as a reflection of the variation of measured loss rates: For instance, Dennis-Smith et al. [2012] note that their oleic acid loss is slower relative to the sub-micron particle studies. Nevertheless, $\alpha_{O3}$ was only varied by $\pm$ 50% to obtain good agreement across this range of measurements, consistent with the experimental uncertainty on such determinations which is usually high. The more significant reduction in $\alpha_{O3}$ for the case of Dennis-Smith et al. [2012] may also be the result of the different experimental approaches. Our composition measurements involve sampling a steady state ozone-exposed aerosol ensemble from a flow tube, while the static chamber set-up used in the single particle study may have required a non-negligible gas phase equilibration time, leading to lower and uncertain ozone concentrations early in the reaction. We also note the different methods of aerosol preparation: in our case, we prepared the aerosol from an OA solution using a nebuliser, while in Dennis-Smith et al. [2012] the aerosol was prepared from the coagulation of homogeneously nucleated OA particles with a sodium chloride “core” particle in the optical trap. Given the combined experimental uncertainty, and possible systematic differences in particle properties, we consider the agreement is very encouraging.

In addition to oleic acid loss from particles, we investigated the particle evaporation behavior presented in Dennis-Smith et al. [2012] using PG-AM. The same chemical scheme as Figure 2 was used again here, and gas-particle partitioning coefficients for oleic acid and each of the C9 products were calculated according to their saturation vapor pressures (Table S1). Dimer products were assumed to be non-volatile.
The model captures the observed size changes over both short and long time scales. The small initial increase in volume (Figure 6(d)), corresponding to only a few nanometers in radius, is explained in the model by the formation of volatile products, particularly nonanal, whose initial evaporation rate from the particle is lower than its production rate. The consequence is an initial build-up of particle-phase nonanal followed by evaporation on longer time scales (Figure 6(e)).

Figure 6: Model simulations compared with observations of oleic acid loss for (a) Dennis-Smither et al., [2012], (b) Hearn et al., [2004] and (c) Ziemann [2005]. We also simulate the single particle volume change of Dennis-Smither et al., (d) at the start of ozonolysis and (e) over the experiment timescale. The model parameters were as for the base case (Table S1) with changes according to the experiment-specific parameters in Table 2. For the simulation in (b), precision and accuracy checks were turned off from Mathematica’s NDSolve routine to allow the model to execute. The experimental data in (c) were obtained directly from P. Ziemann since the Figure presented in Ziemann [2005] contains a small error. These data were offset in time to coincide with the simulated curve and account for the mixing period in the chamber experiment.

The relatively slow initial evaporation of nonanal, despite its high vapor pressure, would be reconciled by a small accommodation coefficient for nonanal and hence slow transfer out of the particle. $\alpha_{org} = 10^{-5}$ was used in the model, which also leads to the gradual evaporation of
nonanoic acid and 9-oxononanoic acid on long timescales after the OA was consumed. This is consistent with the hypothesis of Dennis-Smither et al., [2012] for their continuing particle volume loss. Slow evaporation behaviour may also be a consequence of changes in diffusion within the particle which are not considered in the model. Hosny et al., [2016] observed that the viscosity of oleic acid aerosol increased during ozonolysis, while Lee et al., [2012] hypothesized that an amorphous “crust” formed on the surface of arachidonic acid during ozonolysis, which like oleic acid is an unsaturated, hydrophobic acid. Dennis-Smither et al., [2012] observed a longtime increase in the apparent refractive index retrieved from the evaporating droplet, assuming the particle was homogeneous, even after the size had reached a steady value. This was considered to indicate the possible slow relaxation in a concentration gradient within the particle or a restructuring in particle morphology.

The magnitude of the modelled and measured evaporative losses are comparable over the course of the reaction (Figure 6(e)). However, there is an overprediction of evaporation at short times and slight underprediction at longer times. The model chemical scheme favors formation of nonanal and azaleic acid from the initial cycloaddition reaction; adjusting this branching ratio closer to 1:1 to favor more (semivolatile) nonanoic acid and 9-oxononanoic acid production would reconcile these differences.

We revisit the ozonolysis mechanism to interpret some of the kinetic parameters derived from this model analysis. Decomposition of the unstable primary ozonide (Figure 2(a)) forms the initial functional groups (CI and aldehyde) in close proximity and oriented towards each other, which may promote transient intermolecular interaction between the products. Furthermore, previous studies have noted that the surrounding fatty acid medium is likely to be ordered into a rod-like arrangement of molecules [Iwahashi et al., 2000] owing to the propensity for oleic acid to form hydrogen-bonded acid pairs. These geometric constraints may lead to formation of a “caged” CI-aldehyde complex.

In such a scenario, the CI encounters a high effective aldehyde concentration immediately, whereas other bimolecular reactions require CI reorientation and diffusion. This is a plausible explanation for the much larger 9-ON sink ($k_c$) than for the other C$_9$ products ($k_b$). However, CI
escape must occur to some extent, to explain the latter hydroperoxide products and also secondary ozonides produced by cross reactions from two ozonolysis events, such as \( m/z \) 359.

The slow evaporation of nonanal, represented in the model by a small mass accommodation coefficient, could also be a consequence of restricted escape from such a “caged” geometry. Using a larger value for accommodation (\( \alpha_{\text{nonanal}} \sim 0.1 \)) would require a lifetime for the complex on the order of 10s of seconds to explain the evaporation data. This would appear to be long for a transient complex, possibly suggesting a role for decomposition of initial products (such as oligomers) to yield nonanal, as hinted at by the dimer “sink” reaction discussed in Figure 5(d).

Ultimately, however, the available data do not permit us to distinguish between these hypotheses.

### 4.2. Comparison with other modelling studies

Utilizing a detailed model can provide insight into aerosol processes as demonstrated in the sections above. However, it is important to recognize that the model requires appropriate and physically realistic constraints, specifically in terms of the input parameters used to represent reaction, diffusion and interfacial transport. Our preference is to fix as many of the parameters as possible based on literature values, either from experiment or theory. Fortunately, for the oleic acid-ozone system, a relatively large quantity of relevant parametric data are available and consequently few parameters were optimized by comparison with experimental data. We find that the parameters reported in Table S1 can adequately describe experimental observations within combined experimental and parametric uncertainties.

Similar “fixed parameter” case studies have also proven successful in detailed modelling by Shiraiwa et al. [2010] and Houle et al., [2015] for heterogeneous aging of organic aerosols. An alternative approach which samples more of the model parameter space by globally optimising parameter sets with respect to experimental aerosol measurements has been reported recently [Berkemeier et al., 2016]. This approach may be particularly useful if important parameters are not readily available from the literature for the system of interest. Berkemeier et al., [2016] point out that large experimental data sets are required to adequately constrain degrees of freedom in the model, but we note that even for a relatively well studied system such as the reactive uptake
of ozone to oleic acid particles, appreciable differences in key parameters such as $k_{\text{OA+O}_3}$ can arise ($k_{\text{PG-AM}/k_{\text{Hosny}} \sim 1500}$) [Hosny et al., 2016]. Both approaches may help to assess and constrain relevant physico-chemical aerosol parameters in future.

Conclusions

The combination of measurement and modelling presented in this study represents an important step forward in the detailed understanding of organic aerosol processes, especially for systems such as the ozonolysis of oleic acid aerosol where competition between transport and reaction determines the timescale for atmospheric processing.

The ability of EESI-MS to make aerosol kinetics measurements on a molecular level has been demonstrated for the first time using the ozonolysis of oleic acid aerosol as a model system. Useful quantitative information could be derived from the relative intensities of $[M - H]^{-}$ reactant and product ions in the EESI mass spectra.

A process-level model was used to interpret these measurements and complementary observations from previous studies. Differences in the measured appearance rates of ozonolysis products were used to constrain the relative rates of secondary reactions in the particles. We concluded that the lifetime of Criegee intermediates in the particle was short with respect to isomerization, but that a significant sink for CIs may involve secondary ozonide formation through reaction with the aldehyde group of 9-ON. The reaction between oleic acid and ozone was found to occur in a near-surface layer, in good agreement with experimental studies.

Model performance was further assessed by comparison to other studies with large differences in timescales, ozone concentrations and particle sizes. Chemical and evaporative changes were both reproduced well. Significantly, the chemical insight provided by the new product measurements was used to construct a model chemical mechanism able to successfully explain independent measurements of the evolving particle size. Comparing to multiple experimental observables both improves confidence in the model performance and strengthens the conclusions of experimental work.
The difficulty of interrogating the kinetics of reactive intermediates in particles was demonstrated in this study. This represents an ongoing challenge for the organic aerosol community. Including a mechanism for CI reactions in the model allowed relative rates (e.g. \( k_c/k_a \)) to be assessed and represents a useful starting point. However, since the rate determining step for product formation was the initial ozone-alkene cycloaddition, absolute rates of CI reactions could not be determined. In addition, there are inherent limits to process modelling based on the unavailability or uncertainty of relevant physical parameters for the system under study. Nevertheless, our methodology provides insight into the kinetic regimes and chemical changes associated with organic aerosol aging, and these issues will be addressed in future studies.

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References


